

Microwave-assisted WTB recycling

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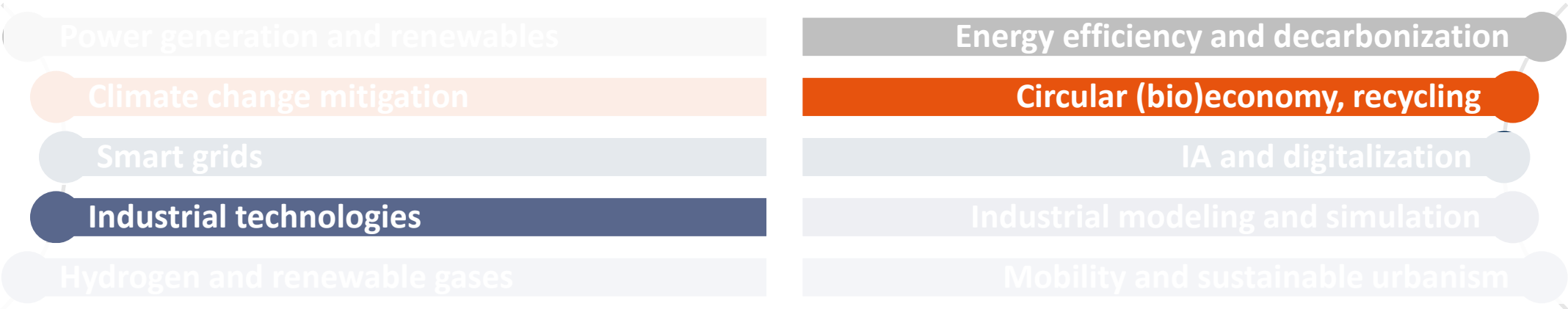
First Stakeholder Workshop

17 November 2026, online event



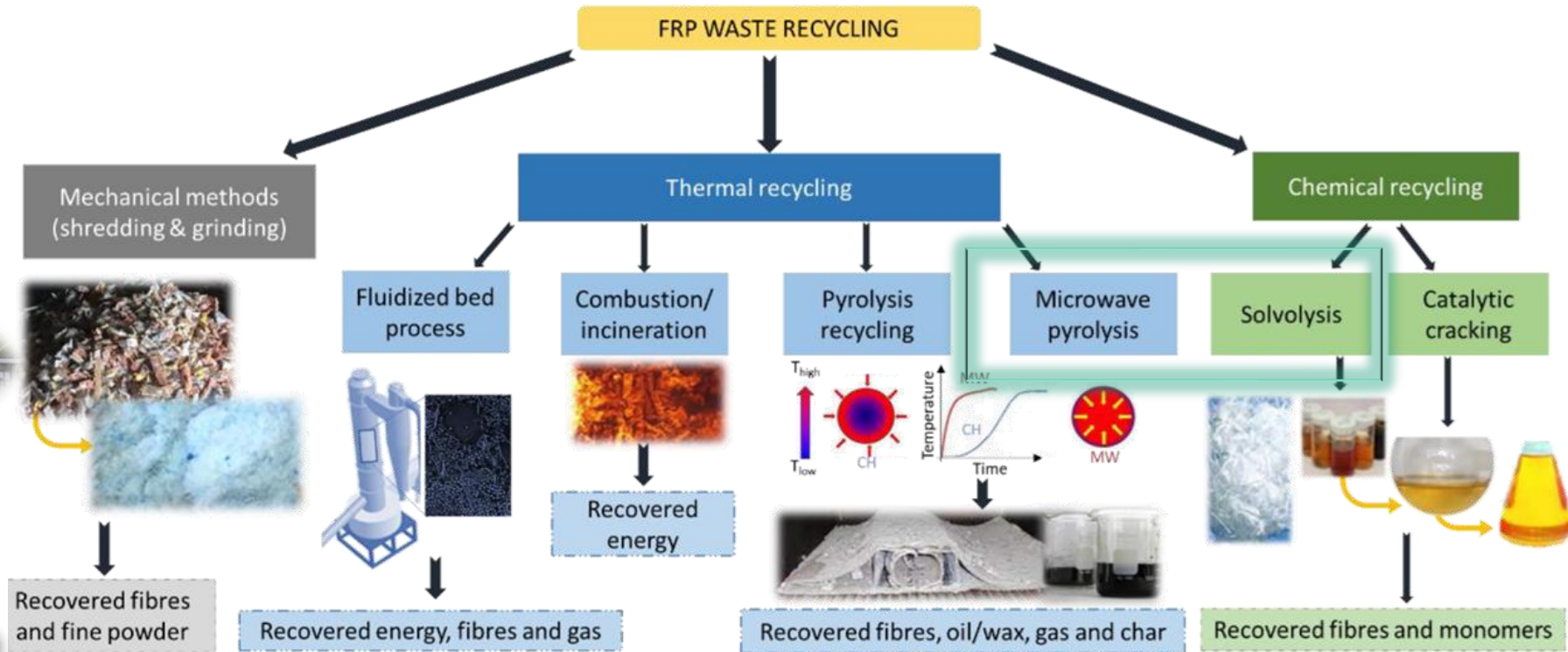


+300	PEOPLE
37,5	AVERAGE AGE
32	PhDs
36%	WOMEN
17	NATIONALITIES



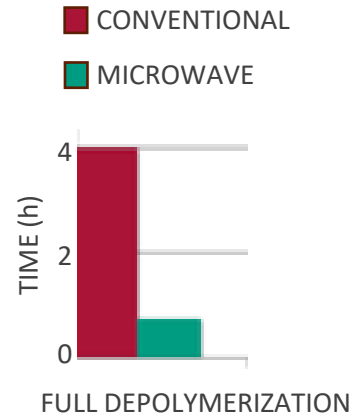
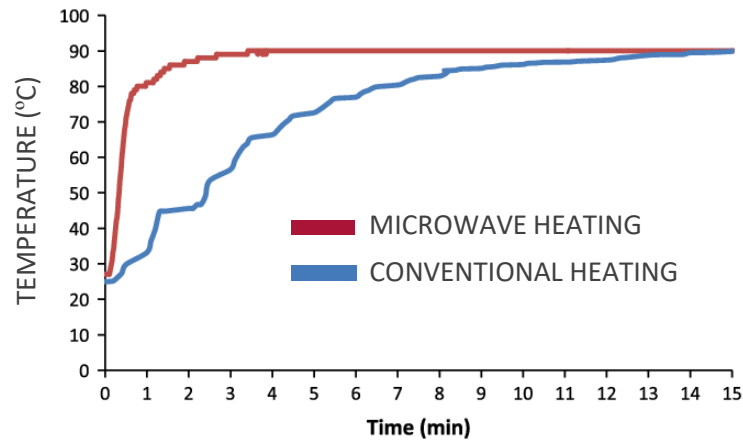
Blades
repurposing

Recycling options for FRP waste from EoL WTB

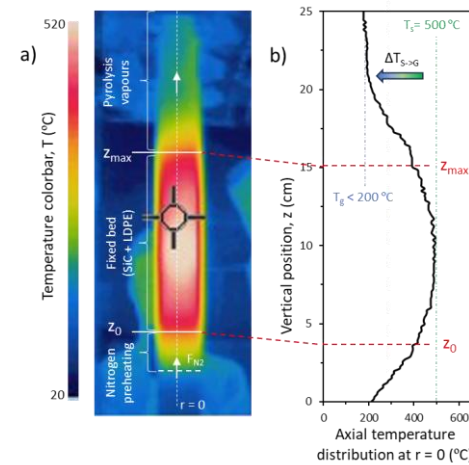


I. Julian et al. Chemical Engineering and Processing - Process Intensification 178 (2022) 109015

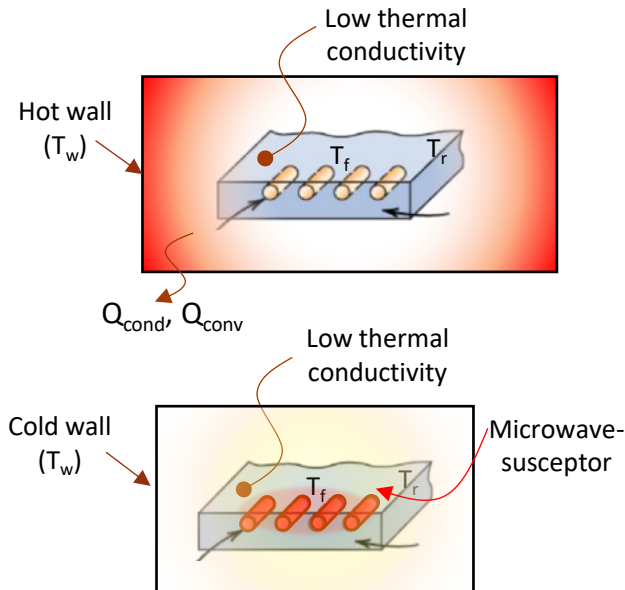
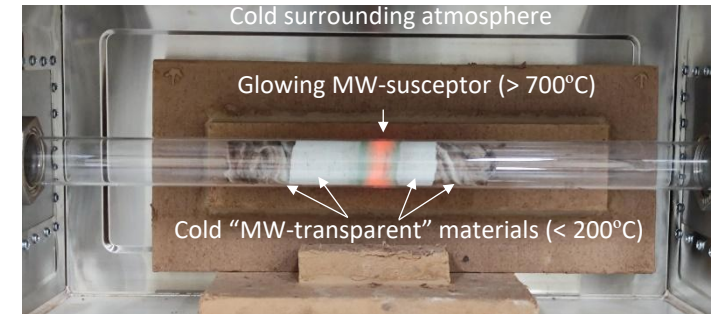
WTB recycling: why using microwaves?



DRASTICALLY REDUCED HEATING & FULL DEPOLYMERIZATION TIMES



GAS-SOLID THERMAL GRADIENTS ON DEMAND



Limitations of conventionally-heated pyrolysis/solvolytic processes:

- Resins heat transfer is very poor: large temperature gradients along the heated medium **limit recycling process controllability**
- Gas-phase cracking in the hot reaction system atmosphere also **limits oil product distribution controllability**

Microwave-assisted heating advantages:

- Fast, selective and volumetric heating
- Enhanced control over pyrolysis process and oil product distribution
- Lower apparent processing temperature for a given depolymerization extent
- Enhanced preservation of mechanical properties of the fibres

MWPYR



MWPYR set-up



Shredded GFRP & SiC
susceptor



Recovered Pyrolyzed
fibers



Isolated pyrolysis oil &
waxes

MWPYR technology	
Configuration	Fixed bed reactor (FBR)
Temperature range	100 – 1000 °C
Max. MW power	3.2 kW
Loading	15 – 20 g GFRP/CFRP 100 – 200 g SiC
Scope	1) Oil & fiber quality characterization 2) Oil yield maximization

MWSOLV



MWSOLV set-up



Reclaimed glass fibers



Washed and dried glass fibers



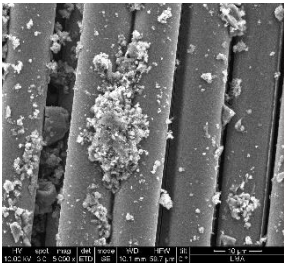
Oil phase

MWSOLV technology	
Configuration	Batch stirred tank reactor (BSTR)
Solvolysis medium	Acid/caustic or organic solvents
Temperature range	150 – 250 °C
Max. MW power	1.5 kW
Pressure range	10 – 80 bar
Loading	30 – 35 g GFRP/CFRP 300 – 350 mL solvolysis medium
Scope	Oil & fiber quality characterization

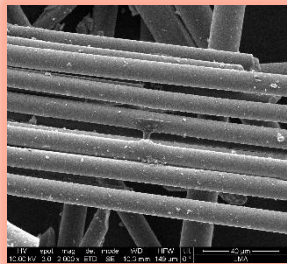
Glass fiber reinforced FRP: MW-PYROLYSIS

Pyrolysis temperature →

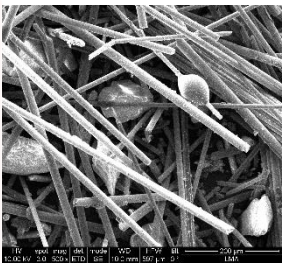
epoxy-FRP



Resin deposits remaining

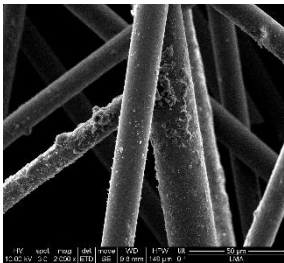


Optimum fibers cleaning

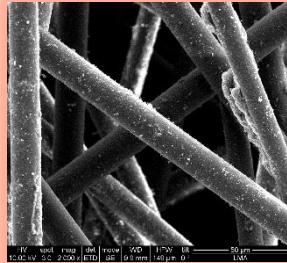


Damaged fibers

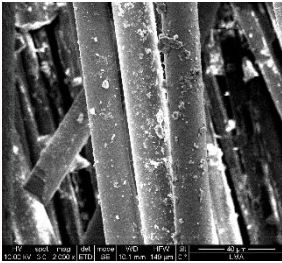
polyester-FRP



Resin deposits remaining



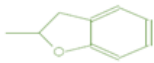
Mid-temp coupled with optimized residence time



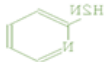
Coke deposits on fibers

epoxy-FRP oils

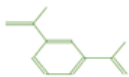
BENZOFURANS



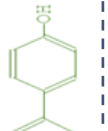
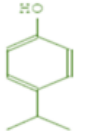
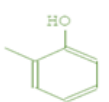
PYRIDINES



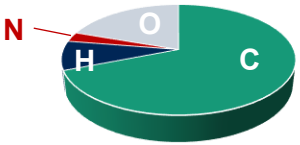
STYRENES



PHENOLS



> 80 wt%

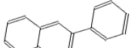
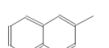


polyester-FRP oils

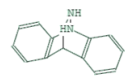
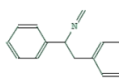
BTX / STYRENES



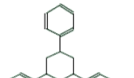
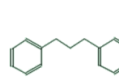
PAH



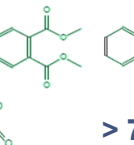
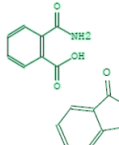
N-PHENYLS



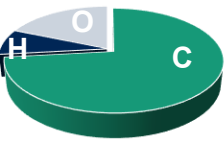
PHENYLS



PHthalates and PHthalic ACID derivatives



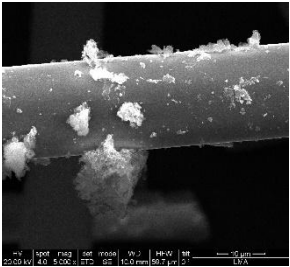
> 70 wt%



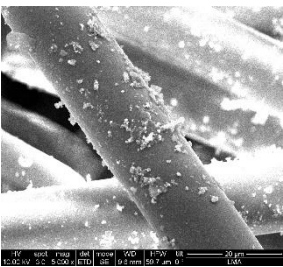
Glass fiber reinforced FRP: MW-SOLVOLYSIS

Solvolyis temperature, catalyst

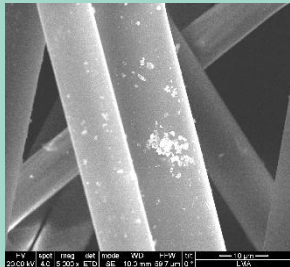
epoxy-FRP



Resin deposits remaining

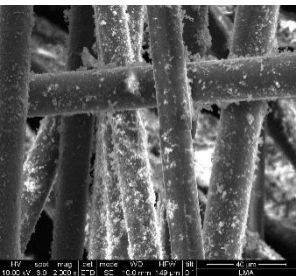


Catalytic salts on surface

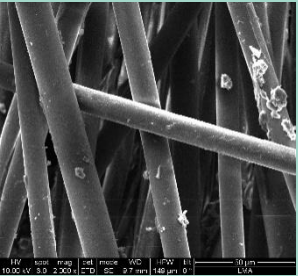


Improved catalyst, fairly cleaned fibers

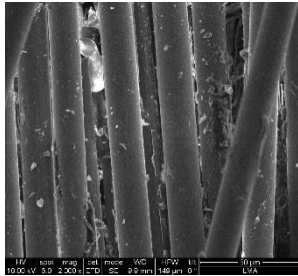
polyester-FRP



Resin deposits remaining



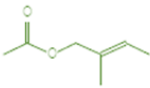
Fairly cleaned fibers



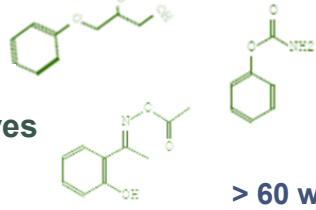
Salt deposits due to catalyst overloading

epoxy-FRP oils

Ester

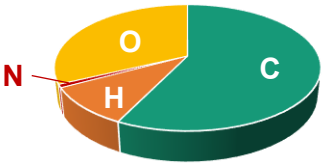


Phenol derivatives



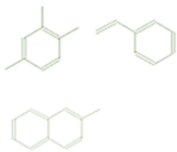
> 60 wt%

Amines

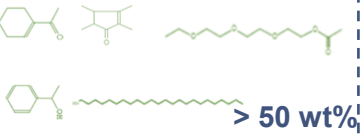


polyester-FRP oils

Linear & Aromatic Hydrocarbons

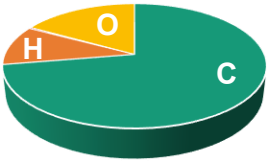
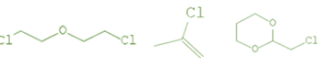


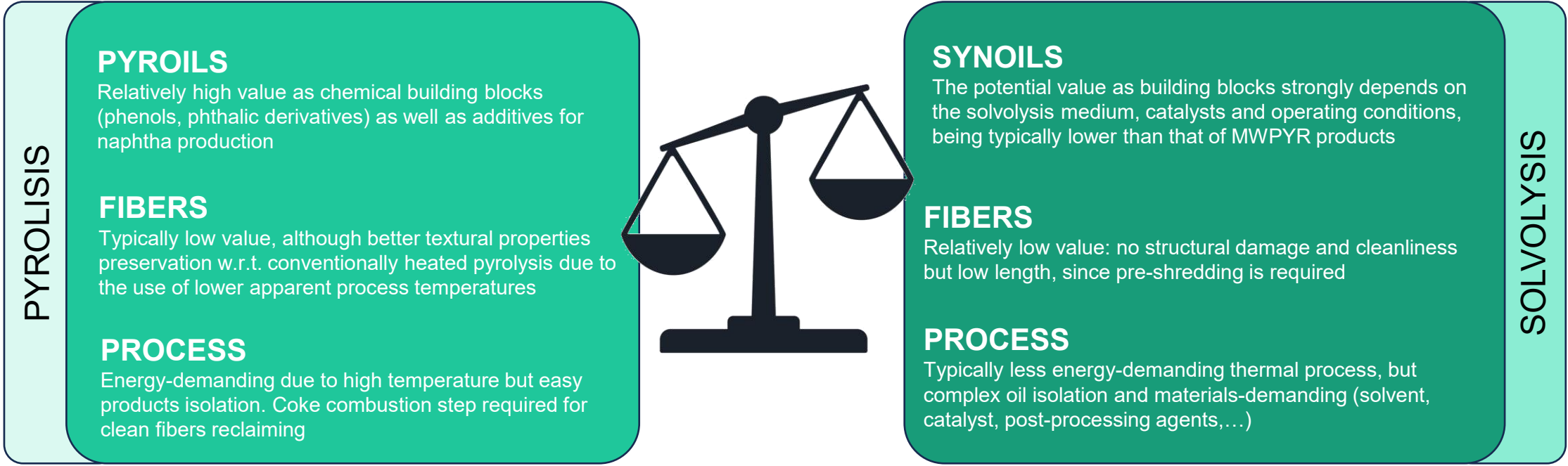
Oxygenated



> 50 wt%

Chlorinated



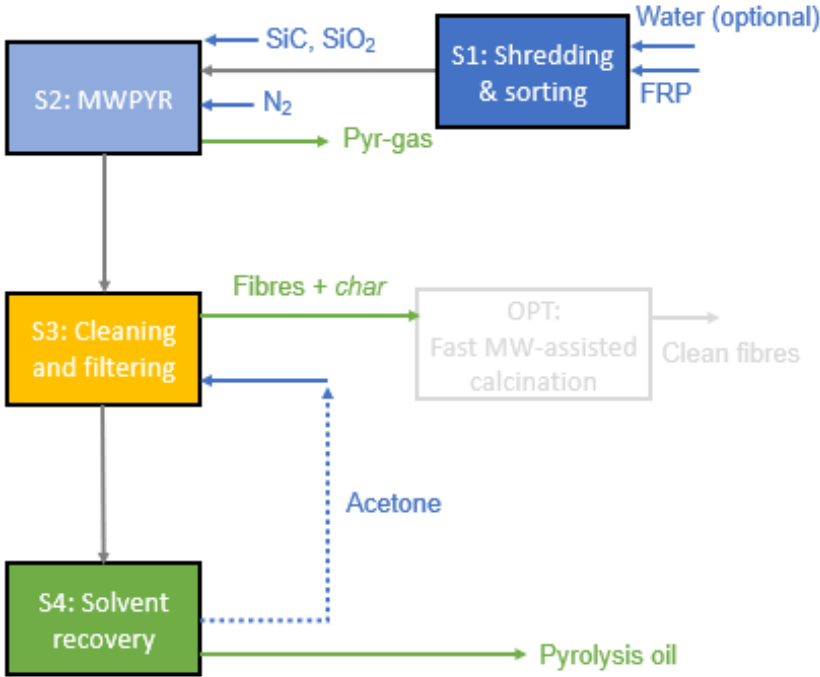


- 1 Which is the most appropriate Technology, among the evaluated ones, from a techno-economic point of view?**
- 2 Is this Technology scalable?

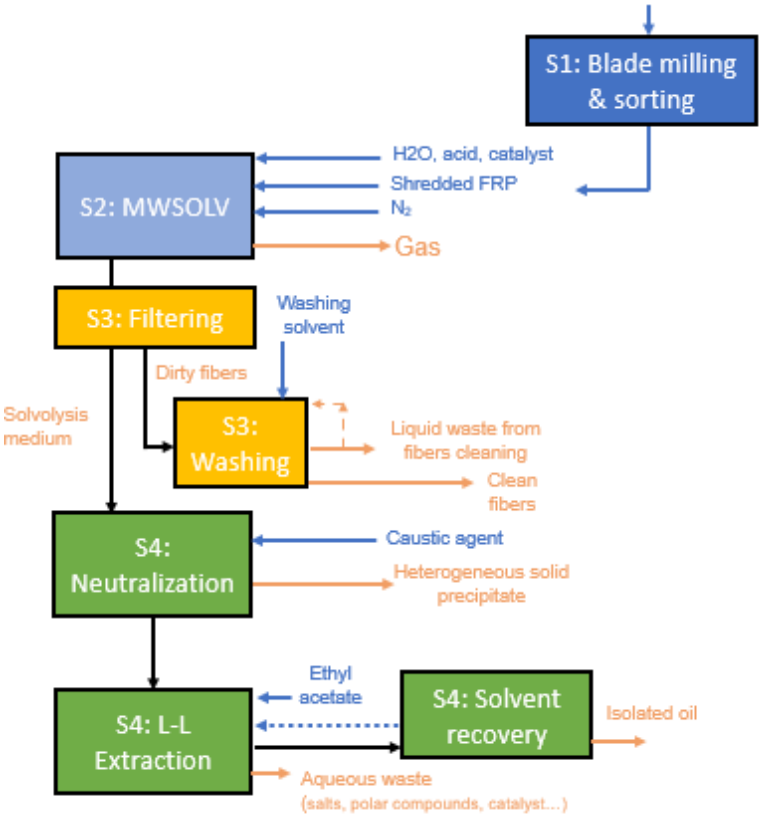
1

Process Flow diagram of MW-assisted thermochemical WTB recycling

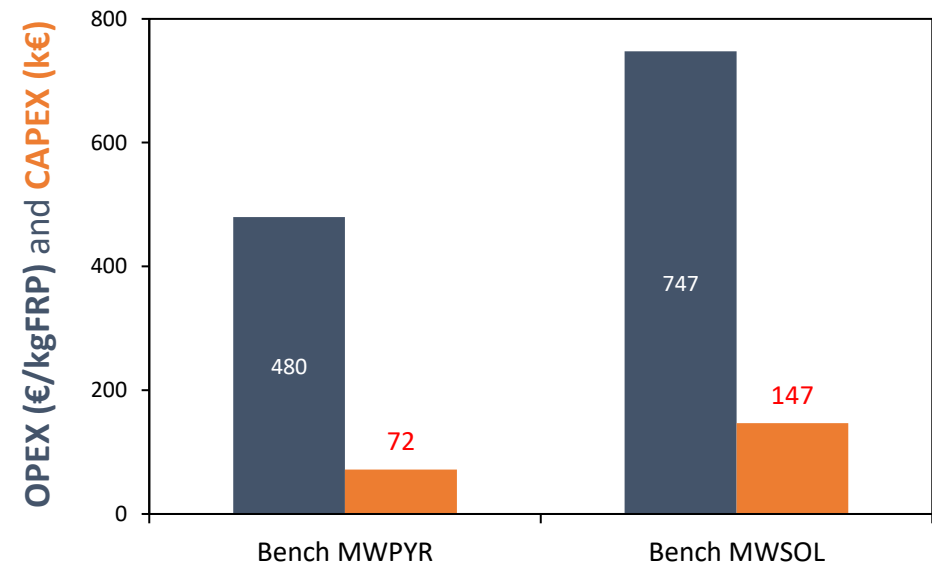
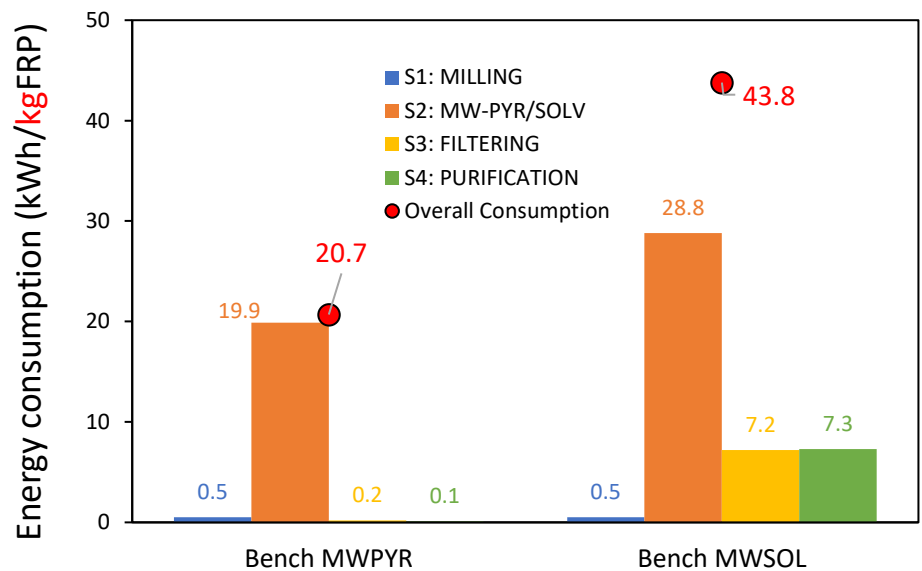
Thermal recycling: MW-pyrolysis



Chemical recycling: MW-solvolyis



1 MW-assisted WTB recycling technologies comparison

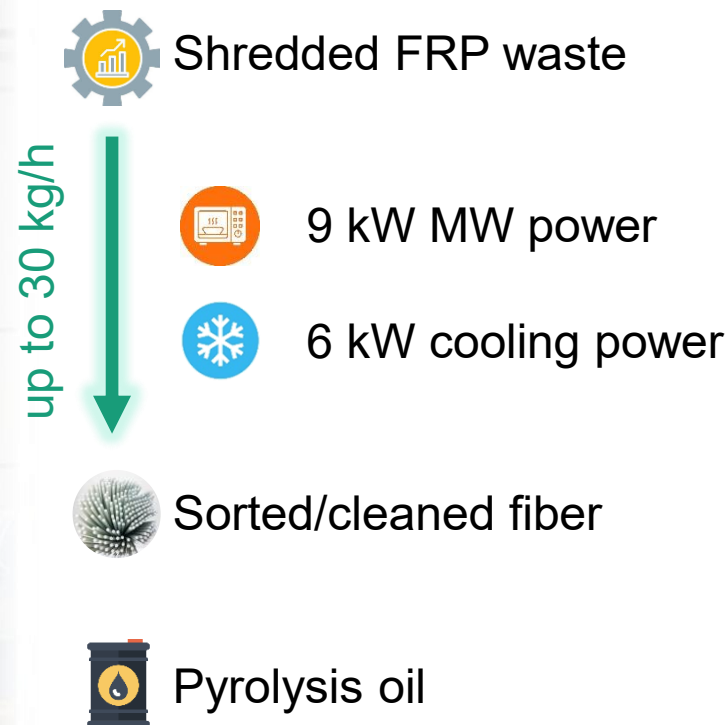


This analysis suggest that **MWPYR outperforms MWSOL** in terms of CAPEX, OPEX and, specifically, process energy consumption. The analysis excludes the **Cost/Benefit** assessment derived from the recycled products' quality and potential selling price.

- 1 Which is the most appropriate Technology, among the evaluated ones, from a techno-economic point of view?
- 2 Is this Technology scalable?

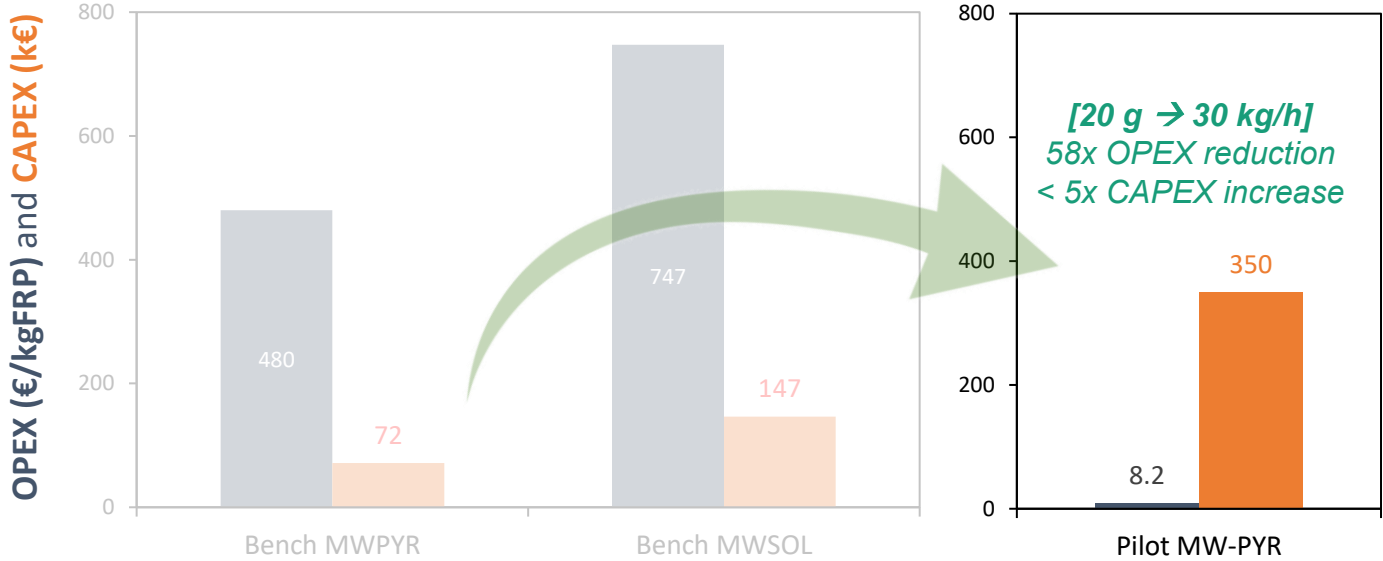
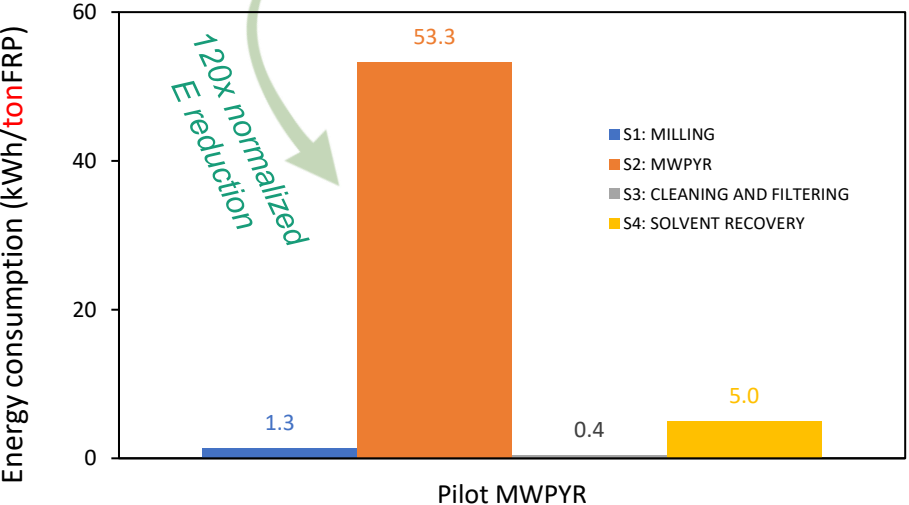
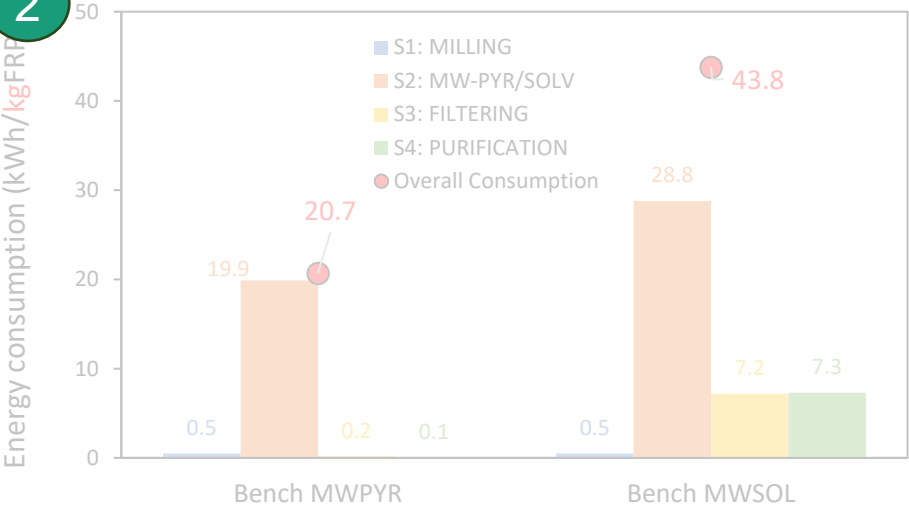
Answers (III)

2



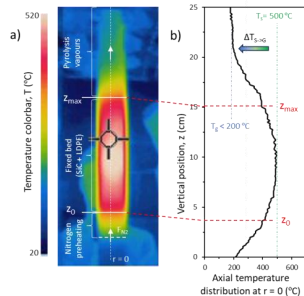
Answers (IV)

2



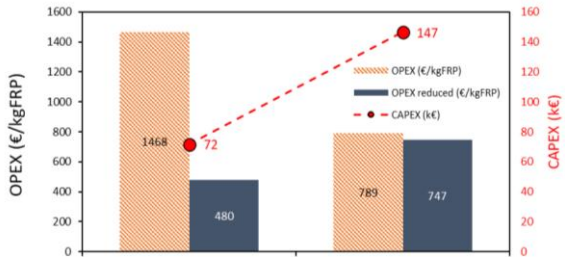
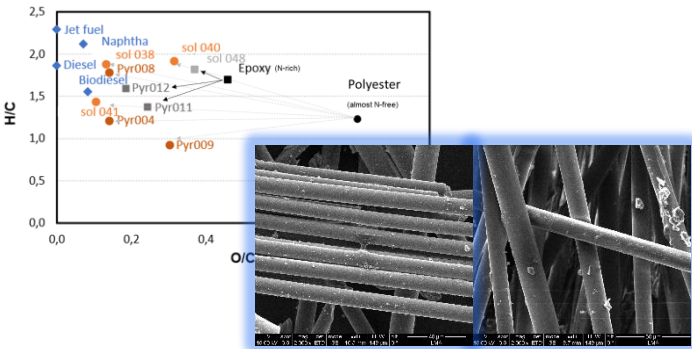
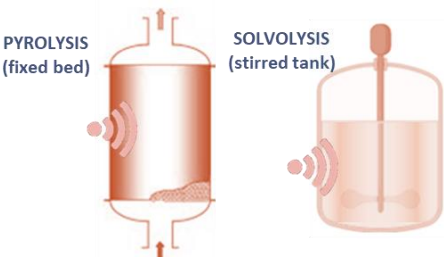
MWPYR process upscaling (continuous operation regime) drastically **increases energy efficiency** and **reduces OPEX**, thus, improving the technology prospects towards industrialization

Conclusions and outlook



Microwave heating boosts **energy-efficiency** of WTB recycling (down to 3x lower consumption per kg_{FRP}), **process controllability** (oil products distribution) and **reclaimed fibers quality** (keeping up to 80% of original mechanical performance)

MW-PYR and **MW-SOL** technologies were experimentally assessed for the thermochemical recycling of FRP from WTB. Both may provide clean GF and/or CF plus complex oils that could be used either as fuels or chemical building blocks



The techno-economic assessment revealed that the **overall cost (CAPEX + OPEX)** of **MW-PYR** is **roughly 2x lower** than that of **MW-SOL**. The quality of the fibers are comparable and pyroils seem more interesting for end-use point of view

A new MW-PYR pilot unit is being commissioned at CIRCE's premises to assess the process scalability and energy efficiency at larger scale under continuous operation. Its maximum (shredded FRP) processing capacity will be ca. 30 kg/h and will be available for bench trials for potential investors





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Thank you for your attention!

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